



A new strategy for catalytic Baeyer–Villiger oxidation of KA-oil with molecular oxygen using *N*-hydroxyphthalimide

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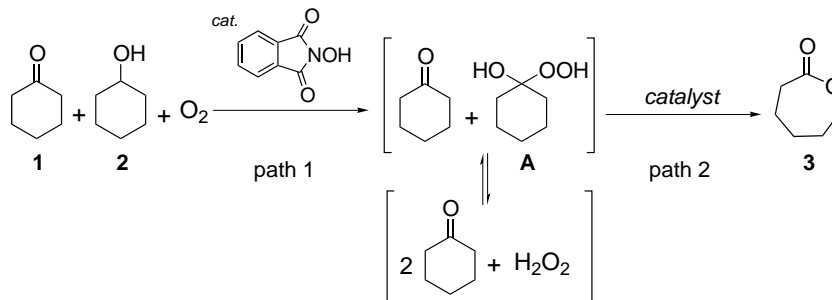
Abstract—Catalytic Baeyer–Villiger oxidation of KA-oil (a mixture of cyclohexanone and cyclohexanol) with molecular oxygen has been developed. The oxidation of KA-oil under dioxygen atmosphere in the presence of a catalytic amount of *N*-hydroxyphthalimide followed by treatment with indium trichloride gave ϵ -caprolactone. © 2001 Elsevier Science Ltd. All rights reserved.

KA-oil, a mixture of cyclohexanone and cyclohexanol obtained by the aerobic oxidation of cyclohexane, is an important intermediate in the petroleum industrial chemistry for the production of adipic acid and ϵ -caprolactam which are key materials for manufacturing 6,6-nylon and 6-nylon, respectively.¹

Baeyer–Villiger oxidation is a frequently used synthetic tool for conversion of cycloalkanones to lactones. Usually, this transformation is carried out by the use of peracids like peracetic acid and *m*CPBA,² hydrogen peroxide,³ and bis(trimethylsilyl)peroxide.⁴ However, the catalytic Baeyer–Villiger oxidation using dioxygen is limited to the in situ generation of peracids using excess aldehydes and O₂.⁵ In industry, ϵ -caprolactone is manufactured by the reaction of cyclohexanone with peracetic acid generated by the aerobic oxidation of acetaldehyde.¹

In previous work, we have shown that *N*-hydroxyphthalimide (NHPI) acts as an efficient catalyst for the aerobic oxidation of various organic substrates.⁶ The NHPI-catalyzed oxidation of secondary alcohols gave ketones through the formation of α -hydroxyhydroperoxide as an intermediate.⁷ From both synthetic and industrial points of view, it is very attractive that the KA-oil can be used as the starting material for the production of ϵ -caprolactone with molecular oxygen via a catalytic process. In this paper, we wish to report a new Baeyer–Villiger oxidation of KA-oil with molecular oxygen under the influence of the NHPI catalyst. To our best knowledge, there are no reports on the catalytic Baeyer–Villiger oxidation of KA-oil using dioxygen as the terminal oxidant.

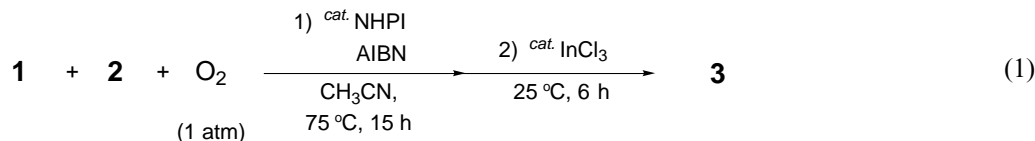
Our strategy is outlined in Scheme 1. The aerobic oxidation of cyclohexanol (**2**) catalyzed by NHPI gives



Scheme 1.

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a mixture of cyclohexanone (**1**) and hydrogen peroxide through the formation of 1-hydroxy-1-hydroperoxycyclohexane (**A**) (path 1). Treatment of the resulting reaction mixture with an appropriate catalyst would produce ϵ -caprolactone (**3**) (path 2). A KA-oil consisting of a 1:1 mixture of **1** and **2** was employed as a model starting material. If the aerobic oxidation of the KA-oil in the presence of NHPI is completed, 2 equiv. of **1** and 1 equiv. of H_2O_2 are expected to be formed.



A standard experimental procedure is as follows: To a solution of NHPI (0.6 mmol) and 2,2'-azobisisobutyronitrile (AIBN) (0.3 mmol) in CH_3CN (3 mL) was added a 1:1 mixture of **1** (6 mmol) and **2** (6 mmol), and then the flask was flushed with dioxygen and equipped with a balloon filled with about 2 L of O_2 . After stirring the reaction mixture at 75°C for 15 h, InCl_3 (0.45 mmol) was added and further stirred at 25°C for 6 h. To decompose the unreacted peroxides, the reaction mixture was treated with excess PPh_3 (10 mmol) at room temperature for several hours. The yields of products were estimated from the peak areas based on the internal standard technique using GC.

Table 1 summarizes the representative results for the Baeyer–Villiger oxidation of the KA-oil. The reaction under standard conditions gave ϵ -caprolactone (**3**) in 57% selectivity based on the KA-oil reacted,⁸ and 77% of KA-oil was recovered (Eq. (1), run 1). This reaction is the first catalytic Baeyer–Villiger reaction of KA-oil with molecular oxygen. The KA-oil recovered includes cyclohexanone **1** as the main component. The same oxidation in the absence of AIBN gave **3** (0.9 mmol) (run 2). Compound **3** was formed in very low yield

without treatment with InCl_3 (run 3). Without treatment of the reaction mixture with PPh_3 , the amount of KA-oil recovered was slightly lowered, because of the presence of unreacted hydroperoxides which are eventually converted into **1** and **2** upon treatment with PPh_3 (run 4). Indeed, the addition of a KI solution to the reaction mixture before treatment with PPh_3 led to color change from light yellow to red–brown, which indicates the presence of peroxy compounds.

Water-stable Lewis acids such as $\text{Sc}(\text{OTf})_3$ and $\text{Gd}(\text{OTf})_3$ were also effective to give **3** in somewhat lower yields (runs 5 and 6). When a protic acid like sulfuric acid was used instead of Lewis acids, peroxy compounds, **4a** and **4b**, derived from **2** and H_2O_2 were formed as major products. It is well-known that **1** reacts with aqueous hydrogen peroxide under neutral and acidic conditions to produce **4a** and **4b**, respectively.^{3a,9}

The oxidation of **2** to **1** was enhanced by the use of the NHPI–Co(II) system,¹⁰ but the formation of **3** was markedly inhibited by the Co ion (run 7). This is believed to be due to the rapid decomposition of the resulting hydroperoxide **A** as well as H_2O_2 by the Co ion, since hydroperoxides undergo the redox decomposition by transition metals.¹¹ The commercially available KA-oil consists of a 1:2.5–4 mixture of **1** and **2**,¹ therefore we examined the oxidation of a 1:2 mixture of **1** and **2**. The reaction under these reaction conditions

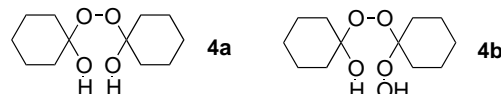


Table 1. Baeyer–Villiger oxidation of KA-oil with molecular oxygen under various conditions^a

Run	Catalyst	Yield of 3 (mmol)	Selectivity of 3 (%) ^b	Recovery of KA-oil (%)	1/2 (mmol/mmol)
1	InCl_3	1.6	57	77	(8.0/1.2)
2 ^c	InCl_3	0.9	60	88	(6.9/3.6)
3	–	0.4	19	83	(8.9/1.0)
4 ^d	InCl_3	1.6	36	63	(6.8/0.8)
5	$\text{Sc}(\text{OTf})_3$	0.7	18	67	(7.1/0.9)
6	$\text{Gd}(\text{OTf})_3$	1.4	40	70	(7.4/1.0)
7 ^e	InCl_3	<1	<1	91	(10.9/0.1)
8 ^f	InCl_3	1.6	57	69	(4.9/1.3)
9 ^g	InCl_3	1.5	60	79	(8.0/1.5)

^a Reaction conditions are shown in text.

^b See Ref. 8.

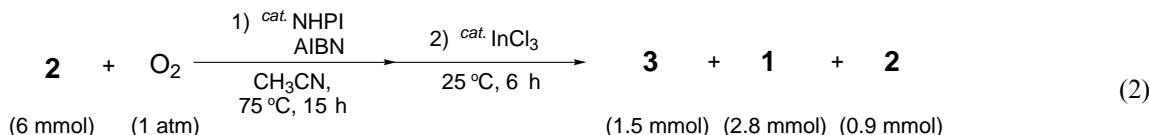
^c Without AIBN.

^d Without treatment of the reaction mixture with PPh_3 .

^e $\text{Co}(\text{OAc})_2$ (0.03 mmol) was added in the step of the aerobic oxidation of KA-oil.

^f A 1:2 mixture of **1** (3 mmol) and **2** (6 mmol) was used.

^g 0.9 mmol of InCl_3 was used.



was found to afford **3** in almost the same yield and selectivity as run 1 (run 8). As expected, similar treatment of cyclohexanol **2** alone with that of the KA-oil led to ϵ -caprolactone **3** and cyclohexanone **1**. The aerobic oxidation of **2** under the influence of the NHPI catalyst followed by treatment with InCl_3 and then PPh_3 afforded **3** (1.5 mmol) and **1** (2.8 mmol) (Eq. (2)).

In conclusion, a catalytic Baeyer–Villiger oxidation of KA-oil with molecular oxygen has first been developed by the use of NHPI as a catalyst. Although the efficiency of the reaction must be improved and more efficient and cheaper catalyst than InCl_3 should be developed, this method may provide an ideal strategy for the production of ϵ -caprolactone **3** from a KA-oil which is a raw material manufactured largely by the aerobic oxidation of cyclohexane.

Acknowledgements

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- The selectivity (%) of **3** was calculated by the following equation.
$$\frac{\left[\frac{\text{the amount (mmol) of } \mathbf{3} \text{ produced}}{\text{the amount (mmol) of starting KA-oil}} \right] - \left[\frac{\text{the amount (mmol) of KA-oil recovered}}{\text{the amount (mmol) of starting KA-oil}} \right]}{\left[\frac{\text{the amount (mmol) of } \mathbf{3} \text{ produced}}{\text{the amount (mmol) of starting KA-oil}} \right]} \times 100$$
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